

Calculating structural and geometrical parameters by laboratory measurements and X-Ray microtomography: a comparative study applied to a limestone sample before and after a dissolution experiment

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Abstract

The aim of this study is to compare the structural, geometrical and transport parameters of a limestone rock sample determined by X-ray microtomography (XMT) images and laboratory experiments. Total and effective porosity, pore size distribution, tortuosity and effective diffusion coefficient have been estimated. Sensitivity analyses of the segmentation parameters have been performed. The limestone rock sample studied here have been characterized using both approaches before and after a reactive percolation experiment. Strong dissolution process occurred during the percolation, promoting a wormhole formation. This strong heterogeneity formed after the percolation step allows to apply our methodology to two different samples and enhance the use of experimental techniques or XMT images depending on the rock heterogeneity. We established that for most of the parameters calculated here, the values obtained by computing XMT images are in agreement with the classical laboratory measurements. We demonstrated that the computational porosity is more informative than the laboratory one. We observed that pore size distributions obtained by XMT images and laboratory experiments are slightly different but complementary. Regarding the effective diffusion coefficient, we concluded that both approaches are valuable and give similar results. Nevertheless, we wrapped up that computing XMT images to determine transport, geometrical and petrophysical parameters provides similar results than the one measured at the laboratory but with much shorter durations.

1 Introduction

Characterizing the rock pore structure such as the porosity, the total pore–rock interface and the connectivity is essential to evaluate oil or gas production or volume of stored CO_2 in case of geological sequestration for example. Porosity is a key petrophysical parameters indicating the total volume of oil, gas or water that can be contained in a reservoir. It is essential to differentiate the total porosity from the open connected or effective porosity, which is the fraction of porosity accessible by any fluid. Connectivity as well as permeability and

tortuosity allow to quantify the ability to extract or inject fluids. The higher the connectivity and permeability are and the lower the tortuosity is, the higher the extraction or injection flow rate will be. In consolidated rock aquifers, the groundwater flow occurs through discrete openings, i.e. fractures, and only to a small extent in the pore-network of the rock matrix. The migration of solutes and solvents in fractured rock aquifers is therefore determined by the relative contribution of advective flow compared to matrix diffusion transverse to the flow direction, resulting in retardation of the solute. The advection transport is controlled by the permeability of the reservoir (mainly controlled by fracture or preferential flow path as wormhole or karst conduit), whereas the diffusion through the matrix depends of the effective diffusion coefficient, which is linked to tortuosity, effective porosity and cementation factor (Archie, 1942; Fick, 1855). Diffusion in rock, of either gas or liquid phase, could be the rate-limiting or dominant process in many scenarios, such as geologic disposal of radioactive waste (Gillham et al., 1984), contaminant remediation (e.g., Becker and Shapiro, 2003), CO₂ geological storage (Hatiboglu and Babadagli, 2010), and oil and gas recovery (Cui et al., 2004, 2009). Diffusion of hazardous gas or liquid chemicals in construction materials has also become a concern for public health and security (Nestle et al., 2001a, b). Therefore, knowledge of diffusion processes and rates in rocks is important to better understand these issues.

To evaluate all these parameters, different laboratory petrophysical techniques are usually used. Some of them are time consuming and destructive methods, such as mercury pore size measurement or BET (Brunauer–Emmett–Teller) surface analysis. Moreover, these different techniques are performed at different sample scales and may require prior preparation, such as thin section for SEM (Scanning Electron Microscope) analysis for example. Yet, most of the laboratories techniques used and discussed in this article are fully validated.

Currently, a lot of petrophysical, geometrical, transport and mechanical parameters are computed using 3-D X-ray microtomography (XMT) images (Alshibli and Reed, 2012). High resolution 3-D XMT is a powerful technique used to image and characterize the internal structure and geometry of natural and/or artificial objects. It is a non-destructive method

that does not need prior sample treatment, such as impregnation, thinning or polishing (Re-meysen and Swennen, 2008). In this technique, contiguous sequential images are compiled to create 3-D representations that may be digitally processed to obtain relevant quantitative geometric and/or morphological parameters (Ketcham and Carlson, 2001). 3-D data provides access to some very important geometric and topological characteristics such as size, shape, orientation distribution of individual features and that of their local neighbourhoods, connectivity between features and network, composition, etc. Computational techniques have progressed to the point where material properties such as conductivity (Arns et al., 2001), diffusivity (Schwartz et al., 1994; Knackstedt et al., 2006; Promentilla et al., 2009; Gouze and Luquot, 2011), permeability (Martys et al., 1999; Arns et al., 2004, 2005a, b), pore size distribution (Dunsmuir et al., 1991; Prodanovic et al., 2010; Garing et al., 2014; Luquot et al., 2014a) and linear elasticity (Roberts and Garboczi, 2000; Arns et al., 2002; Knackstedt et al., 2006) can be calculated on large three-dimensional digitized grids (over 10^9 voxels). More details on this technique, acquisition and data computing step can be found in Taina et al. (2008); Cnudde and Boone (2013) and Wildenschild and Sheppard (2013). In geosciences, the internal structure of a great diversity of geological samples has been examined by radiographic imaging mainly in the last 50 years (Calvert and Veevers, 1962; Hamblin, 1962; Baker and Friedman, 1969; Herm, 1973; Sturmer, 1973; Bjerreskov, 1978; Monna et al., 1997; Louis et al., 2007; Schmidt et al., 2007).

Yet, to our knowledge, no study has been conducted to explore the potential links that can be made between variables computed from XMT images and those traditionally measured in the laboratory for a limestone core rock sample, before and after a dissolution process. Only one similar study was done by Lamande et al. (2013) on soil material using a medical scanner with a large pixel size (0.6 mm). Nevertheless, op. cited authors focused their study to only a few parameters.

Here, we use high resolution X-ray microtomography images to characterize the structural and geometrical parameters of a limestone core rock sample percolated by an acidic solution. We computed and experimentally measured, total and effective porosity, pore size diameter distribution, effective diffusion coefficient, and tortuosity. These parameters are

those needed for numerical modeling to evaluate oil and gas deposit volume and extraction flow rate for example. Quantifying the pore network characteristics of a same sample before and after a dissolution experiment allows to apply our methodology to two different pore networks and enhance the use of experimental techniques or XMT images depending on the rock heterogeneity. The focus of the present study is to articulate the potential of variables estimated using XMT images and how these estimates compare with, and complement, traditional laboratory-based measurements.

2 Materials and methods

In this section, we describe the different laboratory measurements and XMT images computations to evaluate the various petrophysical, geometrical and hydrodynamic parameters. The list of these parameters and the corresponding methods are summarized in Table 1.

2.1 Laboratory methodology

2.1.1 Rock sample

The rock sample used in this study is an oolitic limestone almost composed of calcite (CaCO_3) and is named Bvl in the paper. This limestone is commonly referred to as Beauval rock and is coming from Beaunotte in Dordogne region in France. It is characterized by a beige color with some shells. The mean connected porosity is usually comprised between 9 and 13%, according to general information provided by quarry mining companies. The core sample diameter and length are respectively 2.5 and 2 cm.

2.1.2 Laboratory petrophysical characterization

In order to characterize the different geometrical and structural properties of the rock sample before and after the percolation experiments, we used different classical laboratory ex-

periments. These different techniques have been performed following a home-methodology to avoid too many drying and wetting sample steps.

First of all, to evaluate the effective (connected) porosity, we used the triple weighing method. We first measured the dry sample weight after leaving the sample during 48 h in an oven at 40 °C. We then saturated the sample, starting by a sample vacuum step. Afterwards, we left the calcite equilibrated water penetrate into the pore structure and we weighed the saturated and submerged sample weights. We weighed four times the sample during the dry, saturated and submerged steps. This classical method is very time consuming and requires 4 entire days.

Then, we took advantage of the saturated sample state to evaluate the pore size distribution by measuring the retention curve of the sample using a centrifuge and applying various rotation rates as previously done by Luquot et al. (2014b) and Roetting et al. (2015). The technique consists in applying a high gravity field to an initially saturated sample and measuring the drained volume of water. For this purpose, we used a Rotina® 420R centrifuge following the methodology of Reatto et al. (2008) using 6 speed increments up to 4500 rpm. The maximum suction that can be applied to the sample at 4500 rpm is 213 kPa. This technique allows us to measure the effective capillary size distribution and the retention curve $\theta(P)$, where θ is the volumetric water content and P is the capillary pressure (minus suction). By capillarity theory (Young-Laplace equation with cylindrical approximation), the minimum radius of a pore that drains at P is given by:

$$r_p = \frac{-2\sigma \cos \alpha}{P} \quad (1)$$

where σ is the surface tension ($72.3 \pm 0.5 \text{ mN m}^{-1}$, Adamson and Gast, 1997) and α is the contact angle ($40 \pm 8^\circ$, Espinoza and Santamarina, 2010). Using Eq. (1), we can convert the measured $\theta(P)$ into an equivalent $\theta(r_p)$ curve. This curve is actually a cumulative pore-size distribution; the water content $\theta(r_p)$ indicates the combined volume of all pores with opening radius less than r_p . The measurements were performed twice in the two directions to evaluate the sample anisotropy. Six days were necessary to acquire twice the

retention curves in both directions and dry and saturate again the sample for the second measurement.

After the centrifuge step, we dried the sample again in an oven during 48 h at 40° and measured again the dry sample weight. We then repeated the triple weighing method to evaluate the initial porosity and took advantage of the saturation state of the sample to perform through-diffusion experiment. Classically, the effective diffusion coefficient as well as the tortuosity factor is measured by liquid phase conservative tracer test (usually iodine) as presented by Boving and Grathwohl (2001) and Luquot et al. (2014a).

Through-diffusion experiments were performed to determine the effective diffusion coefficient and tortuosity/constrictivity ratio before and after the dissolution experiment (Li and Gregory, 1974). The same methodology as the one developed by Luquot et al. (2014b) has been used here. The diffusion cell apparatus consisted of two acryl-glass cells of equal size and volume. The reservoir cell contained a 0.02 mol L⁻¹ of potassium iodide tracer solution whereas the sink cell did not contain any tracer at the beginning. We used Beauval rock equilibrated water in both reservoirs and we added several milligrams of sodium azide (NaN₃) to prevent biofilm formation. The mounted rock sample was sandwiched between the sink and reservoir cell. During the experiment, iodide ions diffuse from the reservoir cell into the sink cell through sample Bvl. An iodide-specific electrode from Cole–Parmer Instrument CO was used to measure the iodide concentration in the sink cell. More details about the procedure can be found in Luquot et al. (2014b). The aqueous diffusion coefficient for iodide ($D_{aq} = 1.86 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$) (Robinson and Stokes, 1959) was used to calculate the effective diffusion coefficient D_{eff} . The effective diffusion coefficient was calculated using the equation (van Brakel and Heertjes, 1974; Crank, 1975):

$$D_{eff} = \frac{\beta l}{C_0} \quad (2)$$

where β is the slope of solute mass vs. time, which is obtained from linear regression of data in the steady state range, l is the rock sample thickness and C_0 is the concentration in the reservoir cell. Then, it is possible to determine the tortuosity coefficient using the definition of the effective diffusion coefficient in a porous water-saturated media proposed

by van Brakel and Heertjes (1974):

$$D_{\text{eff}} = \frac{D_{\text{aq}}\phi\delta}{\tau^2} \quad (3)$$

where τ is tortuosity and δ is constrictivity. These coefficients are sometimes gathered together into an empirical exponent m , denoted cementation factor, as in the following equation:

$$D_{\text{eff}} = D_{\text{aq}}\phi^m \quad (4)$$

Through-diffusion experiment are time consuming because of the slow diffusion rate of a liquid tracer, even for porous limestone and sandstone samples (Boving and Grathwohl, 2001). One to two weeks are needed for each measurement.

2.1.3 Laboratory percolation experiment

We performed the flow-through experiment using the apparatus presented in Luquot et al. (2014b). The setup allows to inject at constant flow rate up to four different solutions in parallel through four distinct core samples. Various pressure sensors and a differential pressure sensor enable to monitor the inlet and outlet pressures and then calculate the sample permeability using Darcy's Law. We injected an acidic solution through sample Bv1 at constant flow rate $Q = 16 \text{ mL h}^{-1}$ during 9 h at room temperature and pressure. The injected solution was an acetic acid at $\text{pH} = 3.5$ and buffered at 500 mM. We prepared the injected solution by mixing 28.43 g L^{-1} of acetic acid with 2.184 g L^{-1} of sodium acetate. During the dissolution experiment, we continuously recorded the inlet and outlet pH and the pressure drop between the inlet and outlet of the sample to calculate the sample permeability. The total injected fluid was 146 cm^3 , or some 90 pore volumes of sample Bv1 (initial pore volume = 1.62 cm^3).

Outlet water was sampled periodically, acidified to prevent mineral precipitation, and analyzed for concentrations of Ca using inductively coupled plasma-atomic emission spectrophotometry (ICP-AES, IDAEA, Spain). Reaction progress and porosity changes are cal-

culated from the difference between injected and percolated waters, knowing that calcite is the only mineral composing the sample. Calcite dissolution is described as follows:



. The volume of dissolved calcite ($\Delta V_{\text{calcite}}(t)$) is calculated as:

$$\Delta V_{\text{calcite}}(t) = vQ \int_{t'=0}^{t'=t} \Delta C_{\text{Ca}}(t') dt' \quad (5)$$

where v is the calcite molar volume ($3.7 \times 10^{-5} \text{ m}^3 \text{ mol}^{-1}$), and ΔC_{Ca} is the difference between the outlet and inlet calcium concentration. Therefore, we can calculate the sample-scale porosity change during the percolation experiment using the following equation:

$$\phi(t) = \phi_0 + \frac{\Delta V_{\text{calcite}}(t)}{V} \quad (6)$$

where V is the total sample volume and ϕ_0 is the initial sample porosity. The error $\epsilon(\Delta C_{\text{Ca}})$ in the change of calcium concentration was estimated using the Gaussian error propagation method (Barrante, 1974). The calculated error is propagated to the porosity estimation. After the percolation experiment, we characterized the core rock sample using the same methodology as before, described in Sect. 2.1.2.

2.2 X-ray microtomography images

2.2.1 Images acquisition

X-ray microtomography images were acquired on the ID19 beamline at ESRF (European Synchrotron Radiation Facility), Grenoble (France). The acquisition was done in white beam configuration, using a ROI of 2048×1690 pxls. The sample was placed at 1.7 m and different

filters were used in this configuration (2.8 mm of Al and 0.35 mm of W) to achieve an energy of 71.1 keV with a gap of 57. The voxel size was $7.42 \mu\text{m}^3$. We acquired 4998 radiographies in 360° , 41 references and 20 dark images to reduce the noise during the 3-D reconstruction. The acquisition time for each radiography was 0.25 s which induces a total acquisition time for the entire sample (two scan steps) of about 1 h (taking the motor movements into account). Two 3-D images were acquired: one for the sample before percolation experiment and one after, respectively named Bvl_{be} and Bvl_{af} .

2.2.2 Image processing and parameter extraction

Analysis of the XMT images allows to quantify the volume and morphology of the pore structure identified during the segmentation process. Using the 3-D pore representation, one can estimate its total and connected porosity and geometrical properties, such as its surface area and pore size distribution. The processed images and results were mostly computed with Voxaya's software. The same methodological framework was applied to both images.

Filtering and region of interest extraction

The very first step in the image processing workflow consists in isolating the region of interest: a cylindrical mask is applied on the image in order to extract its relevant part. A median filter is then used to remove noise while preserving edges of the structures.

Segmentation and porosity calculation

Segmentation is one of the most important step in image analysis. It consists in gathering voxels that belongs to a same object and assigning them a single common value ([see Fig. 1 which illustrates the segmentation step](#)). Voxels identified to the matrix constitute the solid phase which have the highest intensity and appear in the brightest gray levels. Pores with size larger than the voxel size (here, $7.42 \mu\text{m}$) are entirely captured by the camera and appear in darkest gray levels in the image, forming a phase referred to as void phase or

resolved porous phase. We name subresolved porous space the area appearing in intermediate gray levels and formed by matrix (calcite in the present case) and pores of size smaller than the voxel size. Note that this phase is sometimes denoted by the ambiguous term “microporous phase” whereas resolved porous phase is often called “macroporous phase”. Presence of pores smaller than the voxel size can be confirmed for example by microscopic observations on thin sections or a priori knowledge of the rock.

In terms of numerical core analysis, computing porosity requires to determine the relative fraction of the void phase volume and to estimate the pore volume in the subresolved porous space. A first segmentation algorithm based on a region growing method was used to isolate the void phase. An additional image segmentation was then conducted to isolate the subresolved porous space and compute its volume fraction in the sample voxel. We can define the sample subresolved porosity Φ_S as:

$$\Phi_S = \xi_x \Phi_x \quad (7)$$

where ξ_x and Φ_x respectively denote the volume fraction and the porosity of the subresolved porous space. The total porosity is then given by:

$$\Phi_T = \Phi_R + \Phi_S \quad (8)$$

where Φ_R is the sample resolved porosity (that is, the volume fraction of the void phase). Assuming that the sample is chemically homogeneous, it is possible to estimate Φ_x . We first compute the mean grayscale values corresponding to solid and void phases, respectively denoted by G_m and G_v . Following (Mangane et al., 2013) and (Luquot et al., 2014a), the gray level value G_x of a voxel belonging to the subresolved porous phase is linearly related to Φ_x as follows:

$$\Phi_x = (G_m - G_x)/(G_m - G_v) \quad (9)$$

Evaluating errors in porosity calculation

Estimating the uncertainty occurring in the porosity calculation can be achieved from an XMT image by performing, for example, several image segmentation with different,

but close, input parameters and then calculating the associated porosities. For instance, if an image is segmented using a basic thresholding technique, then one can perform extra segmentations by varying threshold values by one or two units and computing the associated porosities. This enables to assess the robustness of the segmentation parameters determined by the user.

Connected components of the pore space

A clustering algorithm derived from (Hoshen and Kopelman, 1976) enables to assess the connectivity of the pore space by identifying neighboring voxels that are connected to one another and assigning a distinct label to each connected component. In this study, the largest connected components of the pore space were extracted for both resolved and subresolved porosity.

Geometric parameters

Many geometric parameters can be computed from the segmented image of the pore space, namely the interface surface area, its global curvature and the Euler characteristics (Mecke, 2000; Vogel et al., 2010). Here, we focused on the pore size distribution and the surface-to-volume ratio sometimes referred as specific surface.

The imaged pore space is used to quantify pore network characteristics such as pore size. The pore size distribution is evaluated from XMT images using a Voxaya module. According to (Coker and Torquato, 1995), the pore size distribution function gives the probability that a random point in the pore phase lies at a distance x and $x + dx$ from the nearest point on the pore–solid interface. This is achieved by computing the Euclidean distance from each voxel of the pore space to the interface, using a distance transform algorithm based on Meijster et al. (2002). Equivalently, one can consider this distance as the radius of the largest sphere centered at this voxel and inscribed in the pore space. Yet, each sphere that is fully included in a larger one have no significant contribution to the pore space geom-

etry and can thus be removed. In other words, this method returns the count of inscribed spheres that are maximal in the sense of inclusion.

Statistical measurements such as chord length distribution functions (Torquato, 2002; Luquot et al., 2014a) were also calculated. The chord length distribution function is linked to a probability density of random chords corresponding to a virtual mean pore diameter depending on each x , y , and z direction. It thus provides information on the sample anisotropy.

Diffusion coefficient

Diffusion experiments can be simulated on the void space image following the methodology described in (Sen, 2004). Consider a large number N of (virtual) diffusing particles, initially uniformly distributed in the void phase, and randomly moving following a Brownian motion, the diffusion coefficient $D(t)$ characterizes their ability to disperse in the void phase, probing its structure. We denote by $x_i(t)$ the position of the i th particle at time t and $\sigma(t)^2$ their mean square displacement, that is:

$$\sigma(t) = \frac{1}{N} \sum_{i=1}^N (x_i(t) - x_i(0))^2, \quad (10)$$

Then according to Einstein (1956):

$$\sigma(t)^2 = 6D(t)t \quad (11)$$

If d_0 denotes the diffusion coefficient in an unbounded domain and τ the tortuosity, then when $t \rightarrow \infty$, $D(t)$ tends to an asymptotic value $D \approx d_0/\tau$.

Skeleton and properties

The skeleton of a three-dimensional object is a one-dimensional reduction, centered inside this object, preserving its geometrical and topological features. It provides a simplified representation of a shape: the skeleton of a cylinder, for instance, consists of its axis of rotational symmetry. Formal definitions can be found in Siddiqi and Pizer (2008).

The skeleton is particularly known to be a tool of great interest to investigate large objects with complex geometry, such as large microtomography images of porous media. An implementation of the classical thinning algorithm described in Lee et al. (1994) was used for this work.

3 Results

The temporal evolution of the increase in calcium concentration, ΔC_{Ca} , during the percolation experiment as well as the inlet and outlet fluid pH are presented in Fig. 2. Dissolution reaction occurred during the percolation experiment. Indeed, the ΔC_{Ca} is always positive ($\Delta C_{Ca} > 0$) indicating Ca release in the outlet fluid. Moreover, the outlet pH (Fig. 2) is higher than the inlet one which corroborates proton consumption and thus calcite dissolution (Eq. (R1)). Dissolution reaction may induce porosity increase and other geometrical, structural and hydrodynamical parameter changes. Evaluating and characterizing these changes are essential to develop predictive models of reactive-transport processes such as those occurring during CO_2 geological storage, fracking processes, oil and gas exploitation, acid mine drainage or seawater intrusion among others.

3.1 Laboratory petrophysical parameters

3.1.1 Porosity evolution

Initial porosity measurements on sample Bvl_{be} were performed by the triple weighing method (TW) and give us an initial porosity $\phi_{i(TW)}$ of $16.06 \pm 0.44\%$ (4 measurements), which is slightly higher than the one provided by the quarries miner companies. This porosity is the connected porosity which only takes into account the open pores connected to one of the sample surface. After the dissolution experiment, the same methodology was applied four times and we measured a final porosity $\phi_{f(TW)} = 20.26 \pm 0.73\%$.

Mass balance calculation from the dissolution experiments were performed using Eqs. (5) and (6) and the final porosity was evaluated using the initial porosity $\phi_{f(chem)}$ using the initial

porosity $\phi_{i(TW)}$ and the ΔC_{Ca} presented in Fig. 2. We obtained a final porosity $\phi_{f(chem)} = 19.37 \pm 0.56\%$ (propagating the error of the TW method on the initial porosity value and the one from the chemical analysis). The slightly higher increase in porosity, measured by the TW method, can be explained by the connection of initially non-connected pores to the new connected porosity resulting from the dissolution process whereas the porosity calculated by the mass balance is affected by the dissolution only. The different porosity measurements and calculations are summarized in Table 2.

3.1.2 Pore size distribution

We obtained the pore-size distribution for sample BVI before and after the dissolution experiment from the retention curve (RET) as explained in Sect. 2.1.2. We measured the retention curve by draining the sample both in the flow and counterflow direction in order to evaluate the pore size anisotropy. If the pore-size distribution was heterogeneous, then we should get different retention curves due to the gradient of capillary pressure inside the sample. Specifically, large pores at the inlet (but not at the outlet) will desaturate at small suctions applied to the inlet (i.e., for small rpm when the inlet is placed outside in the centrifuge). Reversely, if the sample is rotated, those pores will only desaturate when suction is large enough to drain any of the outlet pores. The net result is that the measured curve will exhibit directional dependence as previously observed by Luquot et al. (2014b).

Initially, the pore-size distribution is homogeneous; the initial retention curves are similar in both sample orientations (Fig. 3). After the dissolution experiment, due to calcite dissolution and porosity increase, the retention curves vary from the initial one. Moreover, we can observe in Fig. 3, that after the dissolution experiment, some heterogeneity appeared along the sample inducing different shapes for the retention curves acquired in both directions. The corresponding pore-size distributions are presented in Fig. 4.

The results show that after dissolution, the amount of pores of radii larger than $102.27 \mu\text{m}$ increases drastically. The increase in largest pore size is similar whatever the sample direction indicating that these pores are well connected together and broke through the sample. We can also observe (Fig. 3) that the second major difference between the retention curves

before and after dissolution appears for pore radii $10.23 < r_p < 34.99 \mu\text{m}$ (suction between 5.11 et 17.47 kPa). After the dissolution experiment, less pores of such radii are present through the sample, indicating that most of the dissolution occurred in these pores.

The results also display some differences in the pore-size distribution after the dissolution experiment depending on the sample orientation. These differences highlight some heterogeneous dissolution inducing different pore diameter changes along the sample. They are however minor when compared with other experiments with strong dissolution localization (Luquot et al., 2014a). Most discrepancy is visible for intermediate and smallest pores ($0.48 < r_p < 10.23 \mu\text{m}$). Moderately large pores (radius around $10 \mu\text{m}$, suction at 17.47 kPa) are better connected to the inlet than to the outlet (that is, they drain better when the sample is placed opposite to the flow direction, i.e., dragging toward the inlet, than otherwise). The proportion of the smallest pores is consistently lower when the sample is placed opposite to the flow direction, implying that dissolution also occurred in these pores at the inlet. However, the water contents obtained with the sample placed in the flow direction for high suctions (small pore sizes) were higher than before the experiments, implying a small decrease in pore size at the outlet.

3.1.3 Diffusion coefficient

Figure 5 displays the results of the two iodide diffusion experiments performed before and after the dissolution experiment on sample Bv1. The curves show the time evolution of iodide at the sink reservoir, which is proportional to the cumulative mass of iodide that has diffused through the sample Bv1 until time t . Only the steady-state phase is reported here, when the iodide concentration in the sink cell increases linearly with time. Linear regression of the steady state portion yields the effective diffusion coefficient (Eq. 2). Experimental results are summarized in Table 2. After the dissolution experiment, the diffusion coefficient is increased by one order of magnitude, as suggested the noticeable increase in the slope of iodide increment after dissolution. This increase is linked to a decrease of the tortuosity coefficient τ from 14.43 (highly tortuous pore skeleton, see Fig. 6) to 3.57. These values of effective diffusion coefficients and tortuosity, as well as their evolution with dissolution, are

coherent with other previous laboratory measurement done on limestone samples (Boving and Grathwohl, 2001; Gouze and Luquot, 2011; Casteleyn et al., 2011; Peng et al., 2012; Luquot et al., 2014b).

3.1.4 Permeability change

The changes in the sample permeability with time $k(t)$ induced by the dissolution experiment is reported in Fig. 7. Unsurprisingly, permeability increases due to calcite dissolution, as previously mentioned by other authors (Fredd and Fogler, 1998; Luquot and Gouze, 2009; Noiriél et al., 2009; Elkhoury et al., 2013; Carroll et al., 2013). The permeability increase rate (dk/dt) changes drastically at $t \approx 8$ h, which is surely associated with the breakthrough of the main dissolution path (wormhole).

3.2 XMT analysis

3.2.1 Porosity evolution

The total porosity calculated from the XMT images, on sample Bvl_{be} (before dissolution) and Bvl_{af} (after dissolution) is 17.13 % and 22.80 %, respectively. As explained in the methodology section, several steps have been performed with similar parameters in order to estimate the possible error of assessment on this crucial step. We used five different segmentation results to calculate the resolved porosity before and after the dissolution experiment. The results are presented in Table 3. We can observe that decreasing the thresholding value for the sample Bvl_{be} induces a resolved phase underestimation up to 13 % whereas increasing the threshold value only causes an overestimation less than 0.5 %. These calculations indicate that the smallest threshold values were used to estimate the resolved phase volume avoiding huge underestimations. After the dissolution experiment, an error (± 1 and 2) on the thresholding n value carries out less changes on the resolved phase estimation. Increasing and decreasing by 1 the threshold n value after the dissolution experiment has no effect on the resolved phase estimation (error always lower than 0.26 %). Consequently,

all the calculations done on the XMT images were performed using the segmented images obtained by setting the threshold value to n .

Initially, the total porosity calculated on sample $Bv_{l_{be}}$ is characterized by 60.82 % of large pores (resolved porosity) and 39.18% of small pores, lower than the voxel size (subresolved porosity). After the dissolution experiment, the total porosity is mainly characterized by a high amount of large pores (resolved porosity) which represents 68.51 % of the total porosity (see Table 3). The total porosity increase is thus mainly controlled by the increase of the resolved porosity. Figure 8 shows the resolved and subresolved porosities for samples $Bv_{l_{be}}$ and $Bv_{l_{af}}$ along the sample length (which corresponds to the flow direction during the dissolution experiment). We can observe that both resolved and subresolved porosity increase along the sample length. These porosity increases are homogeneous along the sample except for the first millimeters of the sample where the resolved porosity increase faster than in the remaining part of the sample. The same phenomenon is observed for the subresolved porosity, where its increase is higher for the first 2 mm of the sample. Similar trends of porosity increase due to carbonate dissolution have been monitored by previous authors. Nevertheless, no conclusion on the dissolution patterns can be proposed as Luquot and Gouze (2009) and Menke et al. (2015) linked the homogeneous porosity increase profile to homogeneous dissolution whereas Smith et al. (2013) and Luquot et al. (2014a) observed wormhole formation. These versatile conclusions are due to the complex structure and pore geometry of the different limestone samples used. Visualising 3-D XMT images, we can conclude that during Bv_l dissolution experiment a wormhole have been formed promoting a homogeneous porosity increase along the sample.

One of the advantages of using 3-D XMT images is the ability to distinguish the total porosity from the effective one, or in other words from the connected porosity. Performing a connectivity computation, we can evaluate which part of the total porosity is actually contributing to the fluid flow. Table 4 indicates the volumes of the resolved and subresolved phases are indicated as well as the volume of the connected resolved and subresolved phases with the corresponding fraction of the connected part. We can observe that initially, the sample is mainly connected through the subresolved phase, but after the dissolution

experiment the resolved porous phase becomes more connected and mostly contribute to the fluid pathway. This increase in connectivity through the resolved porous phase can be linked to the wormhole formation which represents 71.47% of the connected resolved porous phase. Various other small clusters compose the percolating resolved phase but none of them is larger than 2% of the total porous volume. The main connected path after the dissolution experiment is imaged in Fig. 6.

3.2.2 Pore size distribution

The pore size distribution of the resolved porous phase was calculated for sample BV_{be} and BV_{af} using two different methodologies. We calculated the pore size distribution (Psd) as explained in Sect. 2.2.2, computing the radius of the largest inscribed sphere centered at every point of the pore space, provided it is maximal for inclusion. We also estimated an equivalent pore size distribution by performing statistical measurement and calculating the chord length distribution functions (C-l). The chord length distribution functions for sample BV_{be} and BV_{af} are plotted in Fig. 9 for the 3 directions (x , y , z). Results from both methodology (Psd and C-l) are summarized in Fig. 4 where the pore volume distribution is scaled according to the experimental RET thresholds.

Figures 4 and 9 show that initially, the sample is mainly composed of pores having small and intermediate diameters. Most of the pores are smaller than $204.5 \mu\text{m}$ (69.73%) in diameter and no anisotropy is observed. After the dissolution experiment, the chord-length distribution evolved and a certain anisotropy appears. In sample BV_{af} , the amount of small to intermediate pore diameter decreased significantly to 11.27% of pores smaller than $204.5 \mu\text{m}$ in diameter. Larger pores were formed due to the dissolution process. A significant amount of pores presenting diameters comprised between 1 and 3 mm are measured and pores having a diameter up to 20 mm in the x direction can be found. It corresponds to the local face dissolution at the sample inlet inducing large porosity increase (Figs. 8 and 6).

The pore size distribution (Psd) presents similar results than those obtained by the chord length function. Some discrepancies are observed for sample BV_{be} for the largest pore diameter. With the Psd analysis, the highest pores have a diameter comprised between 70

and 204.5 μm , whereas with the chord length function, we calculated initially lower proportion of these pores and a higher one for the largest pores (diameter higher than 204.5 μm).

3.2.3 Diffusion coefficient

The effective diffusion coefficient $D_{\text{eff(XMT)}}$ before and after dissolution is obtained by computing randomly distributed particles in the rock pores following the method describe in Sect. 2.2.2. Figure 10 displays the results of the two computations performed on $Bv_{\text{l}_{\text{be}}}$ and $Bv_{\text{l}_{\text{af}}}$. The curves show the mean squared displacement (Msd) for an interval time step i . For large time steps, the Msd is linearly dependent to the effective diffusion coefficient (Einstein, 1956). Linear regression of the steady state portion yields the effective diffusion coefficient. The obtained effective diffusion coefficient for $Bv_{\text{l}_{\text{be}}}$ and $Bv_{\text{l}_{\text{af}}}$ are summarized in Table 2. As expected and previously reported in the literature (Gouze and Luquot, 2011; Luquot et al., 2014b), the effective diffusion coefficient increases after limestone dissolution experiments.

4 Comparison and discussion

This section compares the different parameters characterized using, on the one hand, classical laboratory measurements and on the other hand, XMT images. We first compared laboratory measurements and computational analysis duration for each parameter, in order to evaluate which approach is the most time consuming. The complete image processing described in Sect. 2.2.2 have been performed on a workstation equipped with two quad core Intel Xeon CPU X5560 @2.80 GHz and 192 GB DDR3 RAM. We can observe in Fig. 11 that globally, even if the computer used here is not a high end build, the total analysis time for $Bv_{\text{l}_{\text{be}}}$ and $Bv_{\text{l}_{\text{af}}}$ is much shorter using image processing than performing laboratory measurements. The total time needed to extract the different parameters discussed in this article from the XMT images is 23 days, whereas the time required to determine the same parameters using laboratory measurements is 60 days. Moreover, some specific processing (namely skeletonization) were performed using basic, non-optimized implementations of

classical algorithms that can be found in open source software packages such as ImageJ. Besides, in most cases, data extracted from XMT images provided more information than the desired parameters studied in this article. Considering porosity for instance, only effective porosity can be determined by the experimental triple weighing method, whereas both effective and total porosities can easily be calculated from the XMT images. Total porosity can be a key parameter when chemical processes such as dissolution occurred. The final porosity closely depends on the initial effective porosity, the porosity created by dissolution and part of the initially closed porosity that the dissolution process made accessible. Porosity determination with helium pycnometry is a fast and non destructive alternative not used in this study.

However, the main drawback of the XMT image analysis is the high dependence of all parameter on the voxel size. When using different laboratory techniques to measure the desired parameters, various resolution scales can be achieved. For example, the total fluid–rock interface determined by BET measurement has higher resolution than the one determined by XMT images. Specifically, the grain roughness as well as grains smaller than the XMT resolution ($7.42\ \mu\text{m}$) cannot be measured and the water–rock interface area is a priori underestimated.

Nevertheless, for most of the determined parameters, good agreement is observed between the data computed from XMT images and the ones measured experimentally. As observed in Table 2, the initial porosity determined by the triple weighing method is only different from the effective porosity extracted from XMT images by 0.74 %. After the dissolution experiment, the estimated porosity is quite similar even if the difference is more important. The final porosity determined by the mass balance calculation is the lowest one ($\phi_{f(\text{chem})} = 19.37 \pm 0.56\%$). As explained before, the slight difference between the porosity obtained by triple weighing and mass balance calculation can be explained by the connection of initially non-connected pores to the new connected porosity by the dissolution process. Actually, the porosity calculated by the mass balance is only affected by dissolution. In this case, if only initial effective porosity and mass balance are used, the final porosity can be underestimated. Indeed, as observed in Fig. 12 a volume of $32\ \text{mm}^3$ of non-connected

pores is initially present in the final wormhole feature. The porosity measured by the triple weighing method is smaller than the one estimated from the XMT images. This difference can be due to the formation of highly connected pathways (wormholes) percolating the entire core. This very permeable fluid pathway in the sample after the dissolution experiment represents an important water leak pathway where some water can flow out the sample, leading to an underestimation of the saturated sample weighing. Regarding porosity measurement and analysis, we can conclude that porosity calculated from the XMT images is the most reasonable, as we can distinguish the effective one from the total one. Moreover the time required to calculate the XMT porosities is much shorter than the one needed by the triple weighing method.

The same conclusion cannot be drawn for the pore size diameter distribution. For this parameter, the retention curves acquisition allows to classify pores with diameters smaller than the XMT images voxel size ($7.42\ \mu\text{m}$). Figure 4 displays the pore size distributions before and after the dissolution experiment determined by three different methods: measuring the retention curves of the core sample via laboratory experiments (RET), calculating the larger sphere inscribed in the pore space (Psd) and measuring the chord length distribution function (C-I) on the XMT images. As already mentioned, we can see that the pore size distribution obtained by the retention curves analysis allows to determine the quantity of pore with radii down to $0.48\ \mu\text{m}$. Results from Psd and C-I are quite similar. In sample BvI_{be}, the C-I methods determined a higher amount of very large pores whereas the Psd methods estimated larger content of pores with radii comprised between 34.99 and $102.27\ \mu\text{m}$. After the dissolution experiment, for both techniques based on the XMT images the fraction of the largest pores increases significantly. This increase of the amount of large pore is in agreement with the dissolution process and the formation of a preferential flow path (wormhole). Comparing with the RET method, we observed that the RET pore size distribution underestimates the largest pores and the smallest pores are certainly overestimated. This large difference can be attributed to the basic definition of a pore (Nimmo, 2004; Hinai et al., 2014). Indeed, during retention curves measurement, the volume of pore estimated for a given suction pressure correspond to the volume of extracted water through a corre-

sponding throat. Consequently, this laboratory technique gives a mixed estimation between pore and throat distribution, underestimating the largest pores and overestimating the smallest ones. It might be interesting to simulate drainage and imbibition experiments using the XMT images as previously done by Knackstedt et al. (2006) and Prodanovic et al. (2010) in order to compare the laboratory RET measurements in a further study. To summarize, one should note that the pore size distribution obtained by the retention curves indicates the capillary pressure needed to extract a specific fluid volume but without any information about the amount of pores containing this fluid volume and the respective pore diameters. The two other methods used here to extract the pore size distribution using the XMT images allow to determine the pore size diameter at each voxel point with some anisotropy information (C-I technique). Nevertheless, with these two methods, we don't have any knowledge about the connectivity and the accessibility to these pores. Using the extracted skeleton, we can extract both pore and throat distribution and localize them in the 3-D sample. This fourth method gives the best pore and throat size distribution and their localization (Fig. 6).

The third main parameter measured experimentally and using XMT images is the effective diffusion coefficient. By laboratory through diffusion experiments, determination of the diffusion coefficient is time consuming (Fig. 11) and strongly depends on sample length as the diffusion time increases with the squared length. Using the XMT images, the calculation of the effective diffusion coefficient is very efficient and performed in less than 9 min. The results of both methods are presented in Table 2. The values obtained by laboratory measurements and statistical modeling are similar. With both techniques, the effective diffusion coefficient increased after the dissolution experiment by one order of magnitude. Consequently, the tortuosity coefficient decreased after the dissolution experiment and both values for Bv_{be} and Bv_{af} are similar for laboratory measurements and image based computations. The statistical estimation using XMT images is a good option to determine the effective diffusion coefficient as the time needed is 1500 times faster than performing laboratory through diffusion experiments.

5 Conclusions

In this paper, we have shown that microtomographic imaging hardware and computational techniques have progressed to the point where properties such as effective diffusion coefficient, conductivity and pore size distribution can be calculated on large three-dimensional digitized images of real core rock sample. We demonstrated that for most of the parameters studied here, the values obtained by computing XMT images are in agreement with the classical laboratory measurements. For some parameters, such as the porosity, the computational one is the more informative, as one can calculate both total and effective porosity. As discussed here, when dissolution process occurs, the knowledge of the total porosity can be necessary. As the definition of pore is highly discussed in the scientific community, we observed that the pore size distributions obtained by XMT images and laboratory experiments are slightly different. We highlighted advantages and limitations of both approaches: the RET measurement allows to determine the accessible volume for a given capillary pressure, whereas Psd and C-I methods extract the maximum pore volume locally without information of its accessibility. Concerning the effective diffusion coefficient, we observed that both approaches are valuable and similar results are obtained. Nevertheless, the duration of a laboratory through-diffusion experiment is much longer than the time required by the computational option (about 1500 times longer).

As a conclusion, computing XMT images to determine transport, geometrical and petrophysical parameters provide similar results than the one measured at the laboratory in only 23 days instead of 60 days for the laboratory option. Moreover, the studied sample presents both resolved and subresolved porosities, which would be the case for any other type of natural or synthetic porous material, whatever the acquisition technique. Thus, the framework developed in this work is relevant and can be easily applied in many contexts.

Furthermore, new developments are expected in a near future favouring microtomographic imaging at higher resolutions with faster acquisition times allowing dynamical effects to be imaged, Bultreys et al., 2015; Douissard et al., 2012; Landry et al., 2014. Further

developments using the extracted skeleton will also allow to extract the accessible pore volume and the capillary pressure needed to ingress.

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Table 1. Summary of the measured parameters and the corresponding methodologies. (seg.: segmentation, Psd: Pore size distribution, Msd: mean square displacement, TPP: Total Porous Phase, RPP: Resolved Porous Phase, CRPP: Connected Resolved Porous Phase).

Analyzed properties		Lab measurement	Methods of analysis		Analyzed phases
			XMT computing	XMT tools	
Porosity	total volume fraction	–		Voxaya seg. algorithm	TPP
	calculation errors	–		Voxaya seg. algorithm	RPP
Geometric parameters	effective porosity	triple weighing method		clustering algorithm	TPP
	interface surface area	BET		Voxaya algorithm	CRPP
	pore size	retention curves		Psd function and Euclidean distance	RPP
				chord-length algorithm	RPP
Hydrodynamic parameters	diffusion coefficient/tortuosity permeability	through-diffusion experiment pressure drop		Voxaya skeleton algorithm	CRPP
				Msd of virtual particles (Brownian motion)	CRPP
				–	–

Table 2. Determined porosities [%] (final one by mass balance calculation (chem), before and after by triple weighing technique (TW), and before and after as well as total (tot.), effective (open), resolved (res.) and subresolved (subres.) by XMT images (XMT)), effective diffusion coefficients D_{eff} [$\text{m}^2 \text{s}^{-1}$] (from through laboratory experiment (I^-) and XMT images (XMT)), permeability k [m^2] and total fluid–rock interface (from BET measurement and XMT images (Minko)) for samples Bvl_{be} and Bvl_{af} .

	$\phi_{(\text{TW})}$ %		$\phi_{(\text{XMT})}$ %			$\phi_{(\text{chem})}$ %	$D_{\text{eff}(\text{I}^-)}$ $\text{m}^2 \text{s}^{-1}$	$D_{\text{eff}(\text{XMT})}$ $\text{m}^2 \text{s}^{-1}$	k m^2	$S_{(\text{BET})}$ $\text{m}^2 \text{g}^{-1}$	$S_{(\text{Minko})}$ $\text{m}^2 \text{g}^{-1}$
	res.	subres.	tot.	open							
Bvl_{be}	16.06	10.42	6.71	17.13	15.94	–	1.43×10^{-12}	3.75×10^{-12}	4.01×10^{-14}	0.3489	0.0018
Bvl_{af}	20.26	15.62	7.17	22.80	21.75	19.37	2.96×10^{-11}	2.26×10^{-11}	1.16×10^{-12}	–	0.0021

Table 3. Sensitivity analysis of the threshold value n value on the relative fraction of the resolved phase volume (RPV [%]) for samples Bv_{be} and Bv_{af} with the relative error ζ [%].

	n		$n-2$		$n-1$		$n+1$		$n+2$	
	RPV (%)	RPV (%)	ζ (%)	RPV (%)	ζ (%)	RPV (%)	ζ (%)	RPV (%)	ζ (%)	
Bv _{be}	10.42	9.06	-13.05	9.39	-9.82	10.42	0.00017	10.46	0.44	
Bv _{af}	15.62	15.17	-2.90	15.61	-0.06	15.66	0.26	16.84	7.81	

Table 4. Resolved (RPV) and total (TPV) phase volume [mm^3] and connected resolved (connected-RPV) and total (connected-TPV) phase volume [mm^3] with the respective connected resolved (connected-RF) and total (connected-TF) fraction [%].

	RPV (mm^3)	connected-RPV (mm^3)	connected-RF (%)	TPV (mm^3)	connected-TPV (mm^3)	connected-TF (%)
Bv_{be}	1007.76	380.90	37.80	1856.53	1727.78	93.07
Bv_{af}	1511.34	1080.18	71.47	2432.96	2321.12	95.40

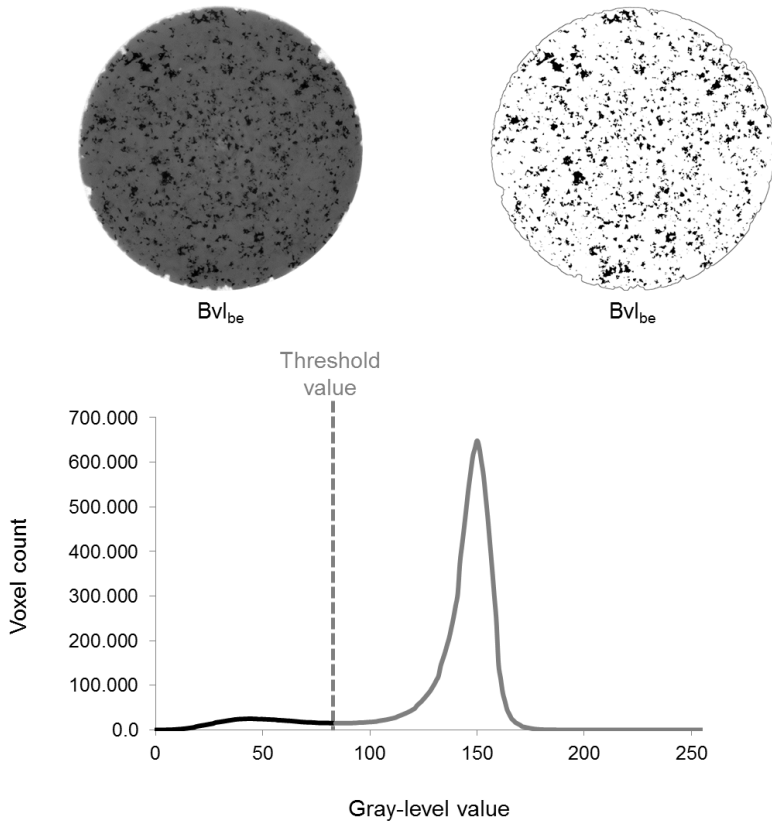


Figure 1. Histogram of gray scale values of Bvl sample images before the dissolution experiment. The threshold value n is indicated in the graph. On the top, a 2D slice of Bvl before the dissolution experiment illustrates the pore initial pore structure on the left and the binary image avec the threshold step on the right.

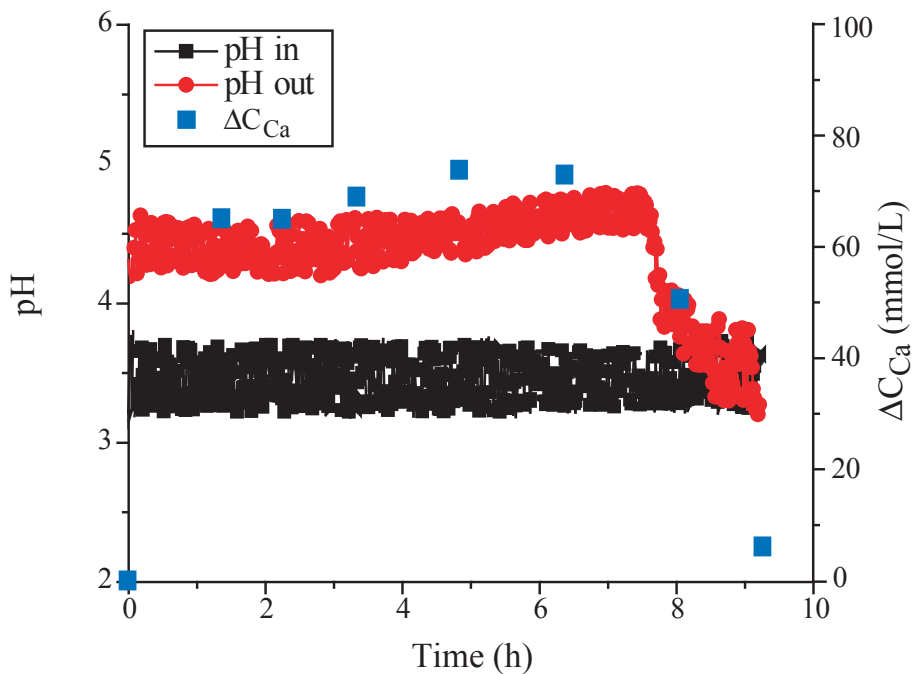


Figure 2. Inlet (black) and outlet (red) pH variation during the percolation experiment as well as variation in calcium concentration (blue).

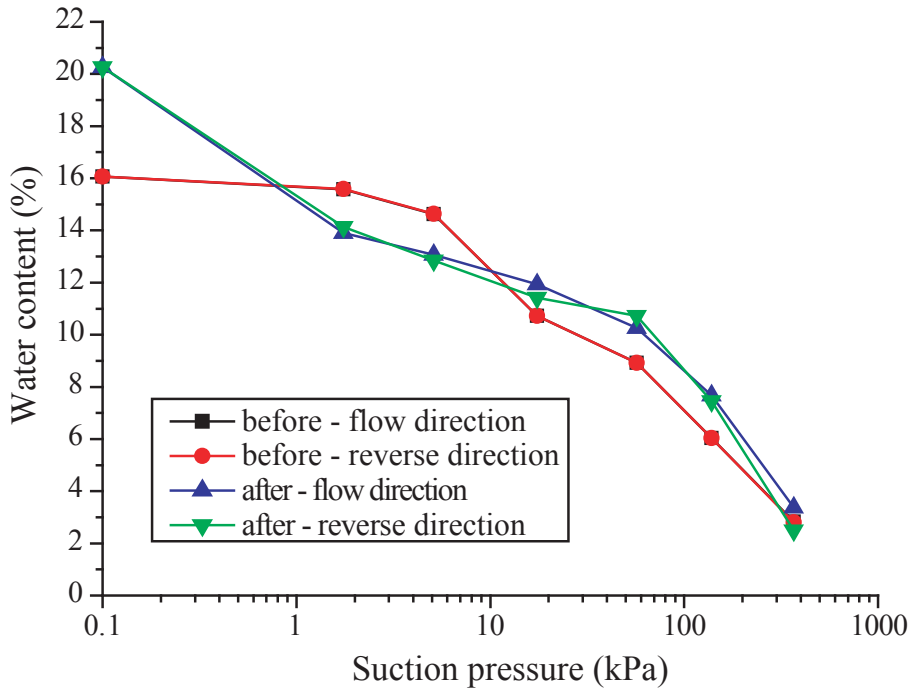


Figure 3. Retention curves before and after the dissolution experiment for sample Bvl.

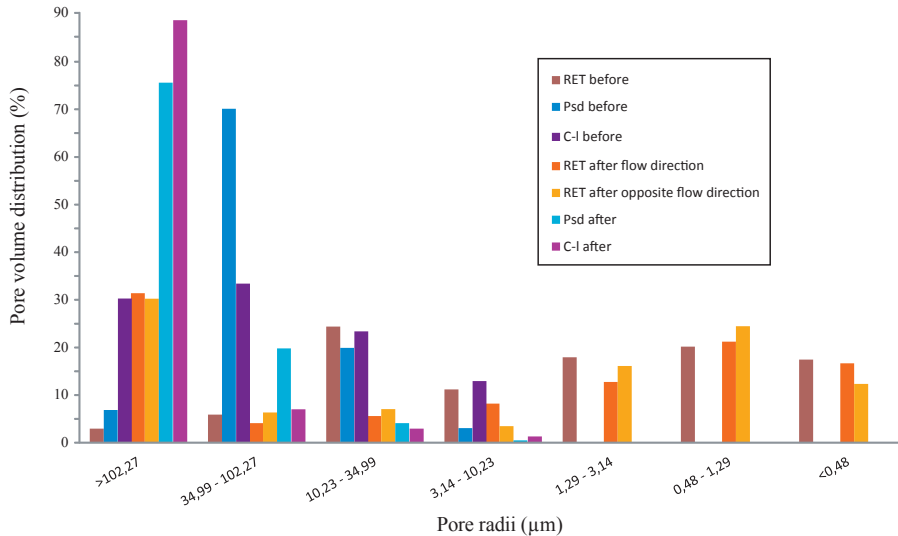


Figure 4. Pore volume content for different pore size diameters before and after the dissolution experiment. The data have been extracted from the Psd and C-I numerical measurements and RET laboratory acquisition. For the latter, the distributions after dissolution were obtained both by draining in the flow direction and in the opposite direction.

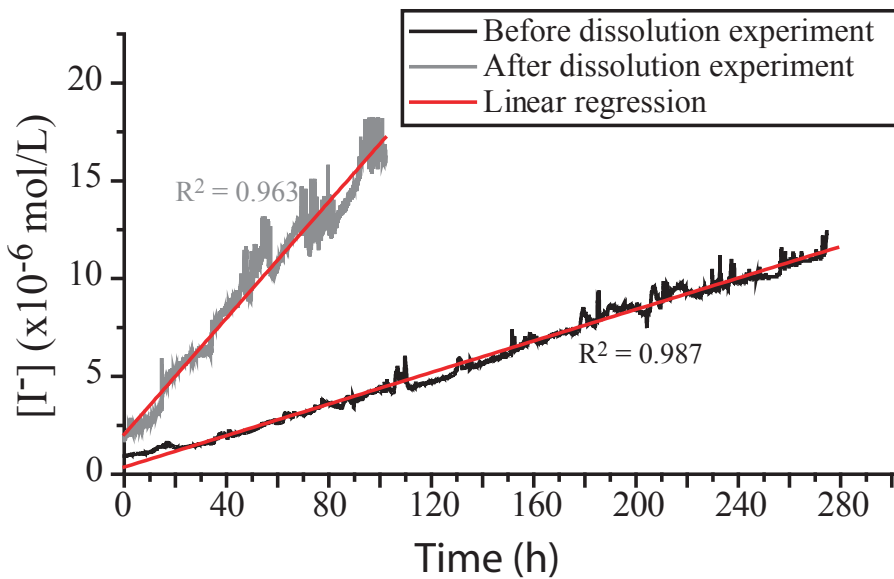


Figure 5. Iodine concentration measured in the sink cell during diffusion experiment through sample BvI before and after the dissolution experiment.

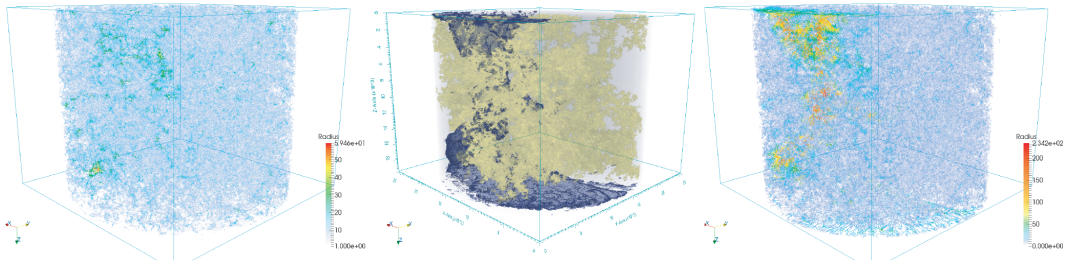


Figure 6. From left to right: extracted skeleton on sample Bvl_{be} , the formed wormholed in sample Bvl_{af} (blue) replaced in sample Bvl_{be} where the resolved connected porosity appears in yellow, extracted skeleton on sample Bvl_{af} . For the extracted skeleton images, the blue to red scale colors corresponds to pore size increase indicated in pixels (up to 60 pxls for sample Bvl_{be} and 234 pxls for sample Bvl_{af}).

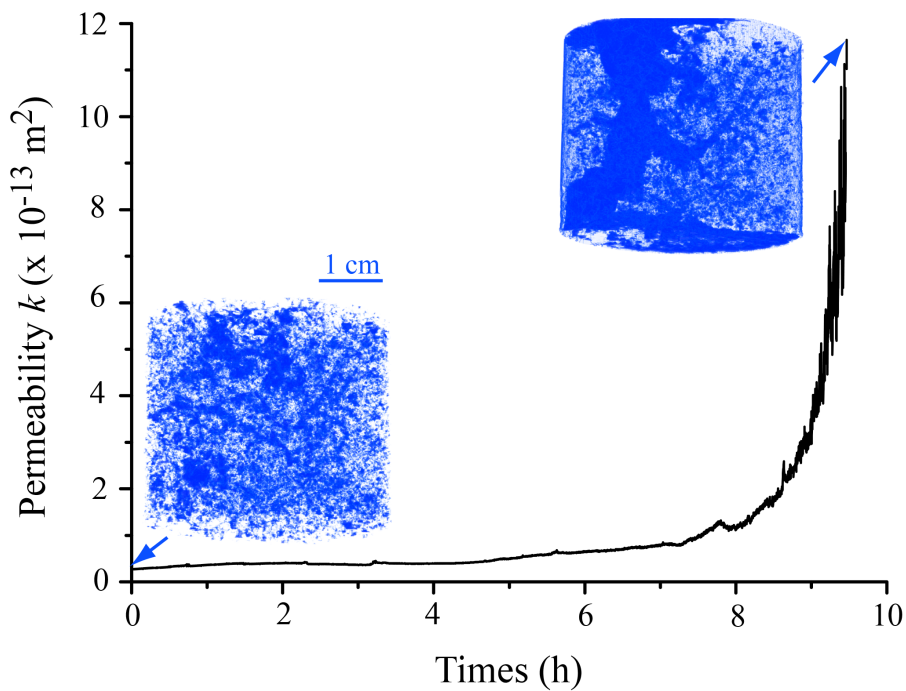


Figure 7. Time evolution of permeability k during dissolution experiment of sample Bvl. The corresponding 3-D images of the resolved porosity for sample Bvl_{be} and Bvl_{af} are reported for the initial and final percolation times.

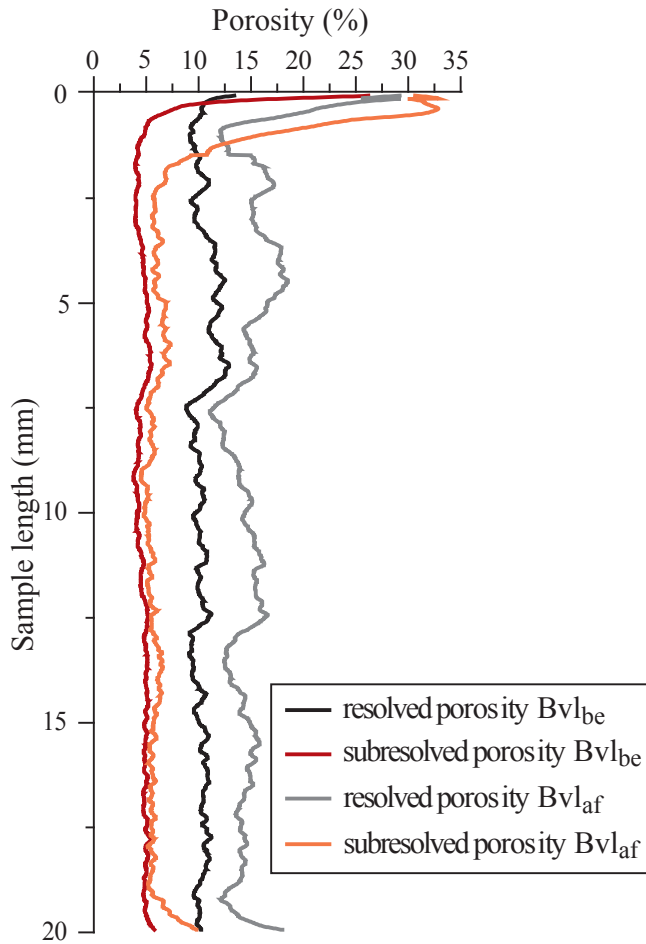


Figure 8. Porosity changes along samples Bvl_{be} and Bvl_{af} . Both resolved and subresolved porosities are plotted.

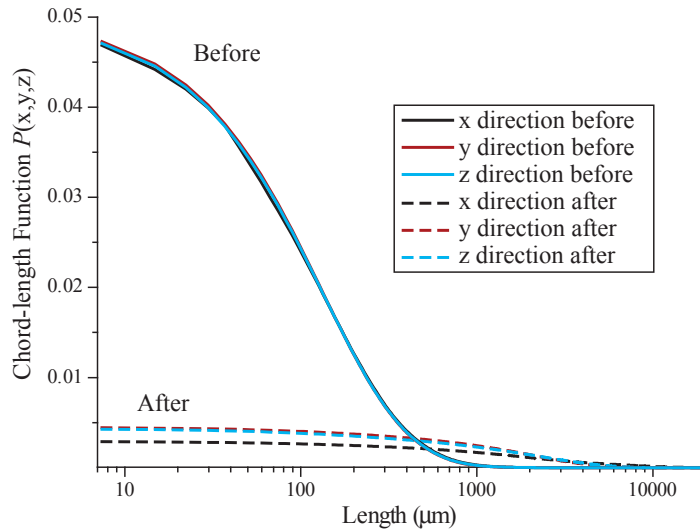


Figure 9. Chord length function along x , y and z ($P(x,y,z)$) for sample BvI before and after the dissolution experiment.

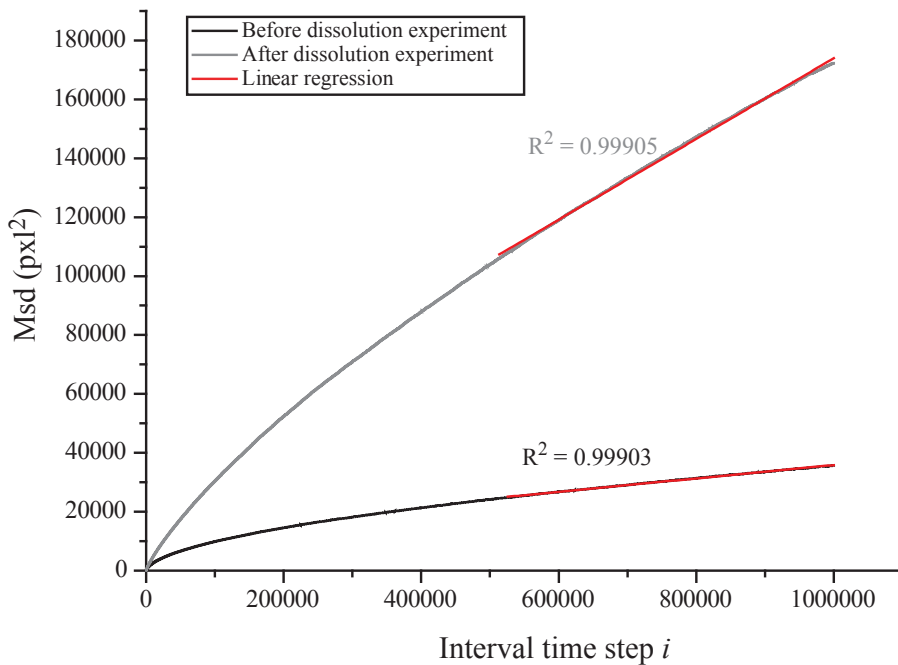


Figure 10. Porosity change along samples Bvl_{be} and Bvl_{af} . Both resolved and subresolved porosities are plotted.

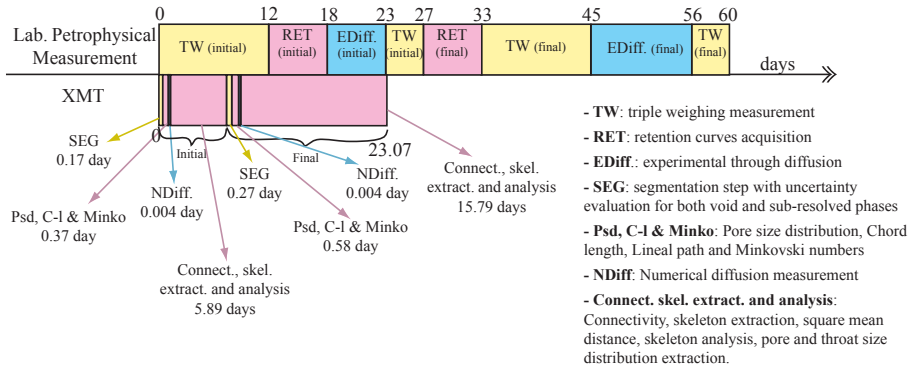


Figure 11. Time scale of the different methods used in this study for both laboratory and XMT images approaches.

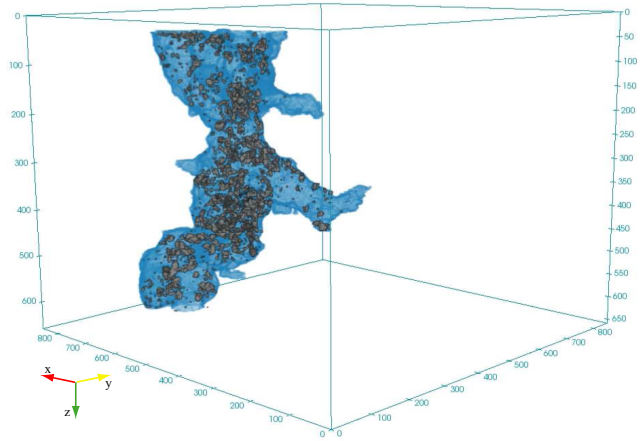


Figure 12. 3D image of the formed wormhole (blue) and initial non-connected porosity presented in the final wormhole feature (gray).